Potential Flow Formulation

Velocity
$$\vec{V} = \nabla \phi$$

Governing Equations for P-Flow

(a) Continuity $\nabla^2 \phi = 0$

(b) Bernoulli for P-Flow (steady or unsteady) $\left| p = -\rho \left(\phi_t + \frac{1}{2} |\nabla \phi|^2 + gy \right) + C(t) \right|$

Boundary Conditions for P-Flow

Types of Boundary Conditions:

(c) Kinematic Boundary Conditions - specify the flow velocity \vec{v} at boundaries.

$$\boxed{\frac{\partial \phi}{\partial n} = U_n}$$

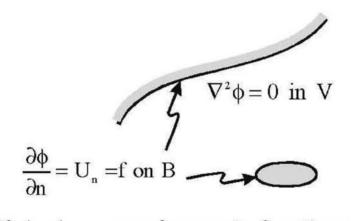
(d) Dynamic Boundary Conditions - specify force \vec{F} or pressure p at flow boundary.

$$p = -\rho \left(\phi_t + \frac{1}{2} \left(\nabla \phi \right)^2 + gy \right) + C \left(t \right) \text{ (prescribed)}$$

Linear Superposition for Potential Flow

In the absence of dynamic boundary conditions, the potential flow boundary value problem is linear.

• Potential function ϕ .

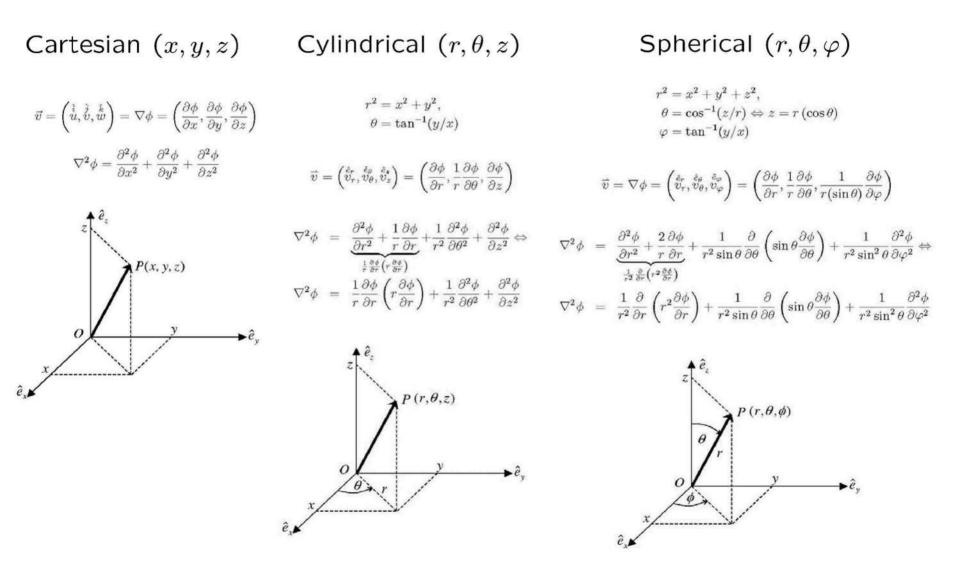


Linear Superposition: if ϕ_1, ϕ_2, \ldots are harmonic functions, i.e., $\nabla^2 \phi_i = 0$, then $\phi = \sum \alpha_i \phi_i$, where α_i are constants, are also harmonic, and <u>is</u> the solution for the boundary value problem provided the kinematic boundary conditions are satisfied, i.e.,

$$\frac{\partial \phi}{\partial n} = \frac{\partial}{\partial n} (\alpha_1 \phi_1 + \alpha_2 \phi_2 + \ldots) = U_n \text{ on } B.$$

The key is to combine known solution of the Laplace equation in such a way as to satisfy the kinematic boundary conditions (KBC).

Laplace Equation in Different Coordinate Systems



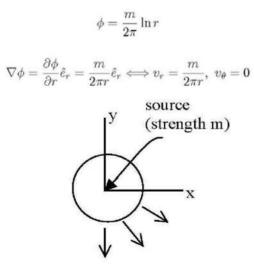
Simple Potential Flows

1. Uniform Stream $\nabla^2(ax + by + cz + d) = 0$

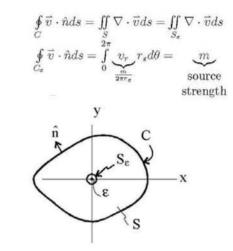
- 2. Source (sink) flow
 - 2D, Polar coordinates

$$\nabla^2 = \frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2}{\partial \theta^2}, \text{ with } r = \sqrt{x^2 + y^2}$$

- An axisymmetric solution: $\phi = a \ln r + b$. Verify that it satisfies $\nabla^2 \phi = 0$, except at $r = \sqrt{x^2 + y^2} = 0$. Therefor, r = 0 must be excluded from the flow.
- Define 2D source of strength m at r = 0:



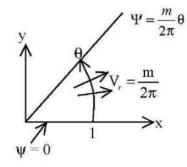
Net outward volume flux is



If $m < 0 \Rightarrow$ sink. Source m at (x_0, y_0) :

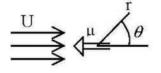
$$\phi = \frac{m}{2\pi} \ln \sqrt{(x - x_0)^2 + (y - y_0)^2}$$

$$\phi = \frac{m}{2\pi} \ln r \text{ (Potential function)} \iff \psi = \frac{m}{2\pi} \theta \text{ (Stream function)}$$



Simple Potential Flows

7. Stream + Dipole: circles and spheres



2D:
$$\phi = Ux + \frac{\mu x}{2\pi r^2} = \cos\theta \left(Ur + \frac{\mu}{2\pi r} \right)$$

The radial velocity is then

$$u_r = rac{\partial \phi}{\partial r} = \cos heta \left(U - rac{\mu}{2\pi r^2}
ight).$$

Setting the radial velocity $v_r = 0$ on r = a we obtain $a = \sqrt{\frac{\mu}{2\pi U}}$. This is the K.B.C. for a stationary circle of radius a. Therefore, for

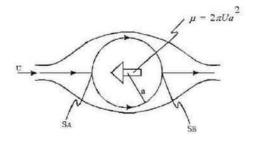
$$\mu = 2\pi U a^2$$

the potential

$$\phi = \cos\theta \left(Ur + \frac{\mu}{2\pi r} \right)$$

is the solution to ideal flow past a circle of radius a.

• Flow past a circle (U, a).



$$\begin{split} \phi &= U \cos \theta \left(r + \frac{a^2}{r} \right) \\ V_{\theta} &= \frac{1}{r} \frac{\partial \phi}{\partial \theta} = -U \sin \theta \left(1 + \frac{a^2}{r^2} \right) \\ V_{\theta}|_{r=a} &= -2U \sin \theta \begin{cases} = 0 \text{ at } \theta = 0, \pi & -\text{ stagnation points} \\ = \mp 2U \text{ at } \theta = \frac{\pi}{2}, \frac{3\pi}{2} & -\text{ maximum tangential velocity} \end{cases} \end{split}$$

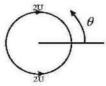
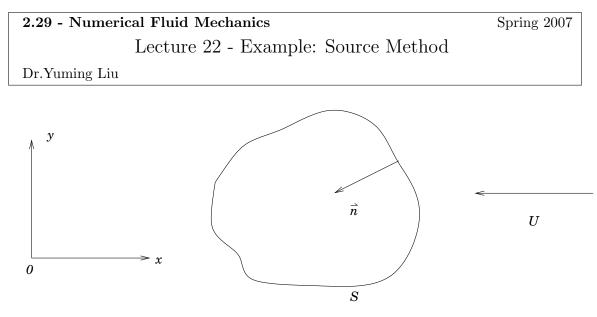


Illustration of the points where the flow reaches maximum speed around the circle.



Boundary-value problem:

$$\begin{split} &\Phi(x,y) = -Ux + \varphi(x,y) \\ &\text{On } S: \ \Phi_n = 0 \qquad \longrightarrow \qquad \varphi_n = Un_x \\ &\text{In the fluid: } \nabla^2 \Phi = 0 \qquad \longrightarrow \qquad \nabla^2 \varphi = 0 \end{split} \tag{0}$$

Source formulation:

$$\varphi(x,y) = \int_{S} \delta(\vec{\xi}) G(\vec{x};\vec{\xi}) ds(\vec{\xi})$$
(1)

 $\delta:$ unknown source distribution on S

 $G(\vec{x};\vec{\xi}) = -ln|\vec{x} - \vec{\xi}|$: 2D Rankine source Green function

From (1), we have:

$$\frac{\partial \varphi(x,y)}{\partial n(\vec{x})} = \int_{S} \delta(\vec{\xi}) \frac{\partial}{\partial n(\vec{x})} G(\vec{x};\vec{\xi}) ds(\vec{\xi})$$
(2)

Substituting (0) into (2), we obtain:

$$\int_{S} \delta(\vec{\xi}) \frac{\partial}{\partial n(\vec{x})} G(\vec{x}; \vec{\xi}) ds(\vec{\xi}) = U n_x \qquad \text{for } \vec{x} \in S \tag{3}$$

To solve (3) numerically for $\delta(\vec{\xi})$, we apply constant panel method:

$$\sum_{j=1}^{N} \int_{S_j} \delta(\vec{\xi}) \frac{\partial}{\partial n(\vec{x})} G(\vec{x}; \vec{\xi}) ds(\vec{\xi}) = U n_x$$
$$\longrightarrow \sum_{j=1}^{N} \delta_j \int_{S_j} \frac{\partial}{\partial n(\vec{x})} G(\vec{x}; \vec{\xi}) ds(\vec{\xi}) = U n_x \tag{4}$$

For $\vec{x} = \vec{x}_i$ and with \vec{x}_i being the position of the centroid of the *i*-th panel and δ_j the source strength of the *j*-th panel, (4) becomes:

$$\begin{split} \sum_{j=1}^{N} \delta_{j} \underbrace{\int_{S_{j}} \frac{\partial}{\partial n(\vec{x}_{i})} G(\vec{x}_{i};\vec{\xi}) ds(\vec{\xi})}_{A_{ij}} &= \underbrace{Un_{x}(\vec{x}_{i})}_{B_{i}} \\ \implies \boxed{\sum_{j=1}^{N} \delta_{j} A_{ij} = B_{i}}_{A_{ij}} \quad i = 1, 2, \cdots N \\ \longrightarrow \quad [A]\{\delta\} = \{B\} \\ A_{ij} &= \int_{S_{j}} \frac{\partial}{\partial n(\vec{x}_{i})} G(\vec{x}_{i};\vec{\xi}) ds(\vec{\xi}) = n_{x}(\vec{x}_{i}) \cdot \int_{S_{j}} G_{x}(\vec{x}_{i};\vec{\xi}) ds(\vec{\xi}) + n_{y}(\vec{x}_{i}) \cdot \int_{S_{j}} G_{y}(\vec{x}_{i};\vec{\xi}) ds(\vec{\xi}) \end{split}$$

After $\{\delta\}$ is obtained:

$$\varphi(\vec{x}_i) = \int_S \delta(\vec{\xi}) G(\vec{x}_i; \vec{\xi}) ds(\vec{\xi})
= \sum_{j=1}^N \int_{S_j} \delta(\vec{\xi}) G(\vec{x}_i; \vec{\xi}) ds(\vec{\xi})
= \sum_{j=1}^N \delta_j \int_{S_j} G(\vec{x}_i; \vec{\xi}) ds(\vec{\xi})$$
(5)

Tangential velocity:

$$\begin{aligned} \varphi_{\tau}(\vec{x}_{i}) &= \frac{\partial}{\partial \tau} \varphi(\vec{x}_{i}) = \int_{S} \delta(\vec{\xi}) \frac{\partial}{\partial \tau} G(\vec{x}_{i};\vec{\xi}) ds(\vec{\xi}) \\ &= \int_{S} \delta(\vec{\xi}) \left[\tau_{x} G_{x}(\vec{x}_{i};\vec{\xi}) + \tau_{y} G_{y}(\vec{x}_{i};\vec{\xi}) \right] ds(\vec{\xi}) \\ &= \sum_{j=1}^{N} \delta(\vec{\xi}) \left[\tau_{x}(\vec{x}_{i}) \int_{S_{j}} G_{x}(\vec{x}_{i};\vec{\xi}) ds(\vec{\xi}) + \tau_{y}(\vec{x}_{i}) \int_{S_{j}} G_{y}(\vec{x}_{i};\vec{\xi}) ds(\vec{\xi}) \right] \end{aligned}$$
(6)

Total Tangential velocity:

$$\Phi_{\tau}(\vec{x}_i) = -U\tau_x(\vec{x}_i) + \varphi_{\tau}(\vec{x}_i)$$

Pressure:

$$\begin{split} \frac{P-\rho_{\infty}}{\rho} &= -\left[\frac{\partial \Phi^{\prime}}{\partial t} + \frac{1}{2}\nabla \Phi \cdot \nabla \Phi\right] + \frac{1}{2}U^2\\ &= -\frac{1}{2}\left[\Phi^{\prime}_n + \Phi^2_{\tau}\right] + \frac{1}{2}U^2\\ \therefore (P-\rho_{\infty}) &= -\frac{\rho}{2}\left[\Phi^2_{\tau} - U^2\right] \end{split}$$

Analytic Solution: (for a circular cylinder of radius R)

$$\varphi(\vec{x}) = -Ux \qquad \qquad \text{for } \vec{x} \text{ on } S$$

$$\Phi_{\tau}(\vec{x}) = 2U\sin\theta \qquad \qquad \text{for } \vec{x} \text{ on } S$$

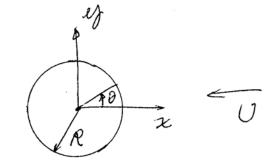
$$C_{\rho} = \frac{P - \rho_{\infty}}{\frac{1}{2}\rho U^2} = 1 - 4\sin^2\theta$$

Cylinder.dat X -

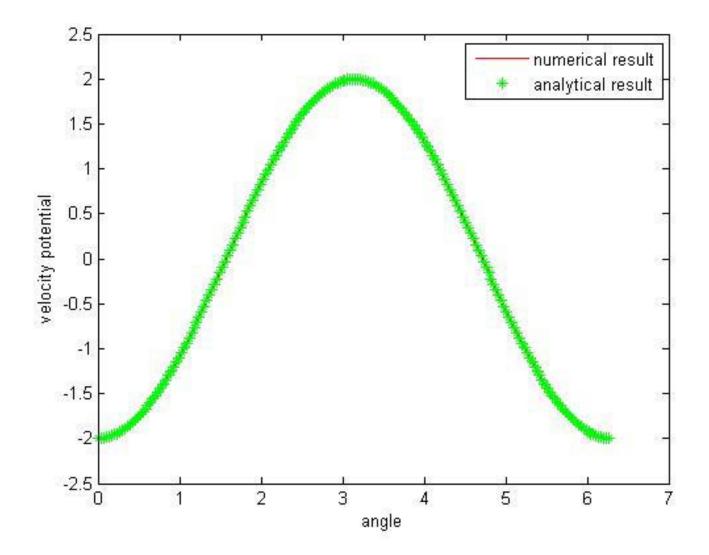
50

2 0000	0 0000
2.0000	0.0000
1.9842	0.2507
1.9372	0.4974
1.8596	0.7362
1.7526	0.9635
1.6180	1.1756
1.4579	1.3691
1.2748	1.5410
1.0717	1.6887
0.8516 0.6180 0.3748 0.1256 -0.1256 -0.3748 -0.6180 -0.8516 -1.0717	1.8097 1.9021 1.9646 1.9961 1.9646 1.9021 1.8097 1.6887
-1.2748	1.5410
-1.4579	1.3691
-1.6180	1.1756
-1.7526	0.9635
-1.8596	0.7362
-1.9372	0.4974
-1.9842	0.2507
-2.0000	0.0000
-1.9842	-0.2507
-1.9372	-0.4974
-1.8596	-0.7362
-1.7526	-0.9635
-1.6180	-1.1756
-1.4579	-1.3691
-1.2748	-1.5410
-1.0717	-1.6887
-0.8516	-1.8097
-0.6180	-1.9021
-0.3748 -0.1256 0.1256 0.3748 0.6180 0.8516 1.0717 1.2748 1.4579	-1.9646 -1.9961 -1.9646 -1.9021 -1.8097 -1.6887 -1.5410 -1.3691
1.6180	-1.1756
1.7526	-0.9635
1.8596	-0.7362
1.9372	-0.4974
1.9842	-0.2507
2.0000	-0.0000

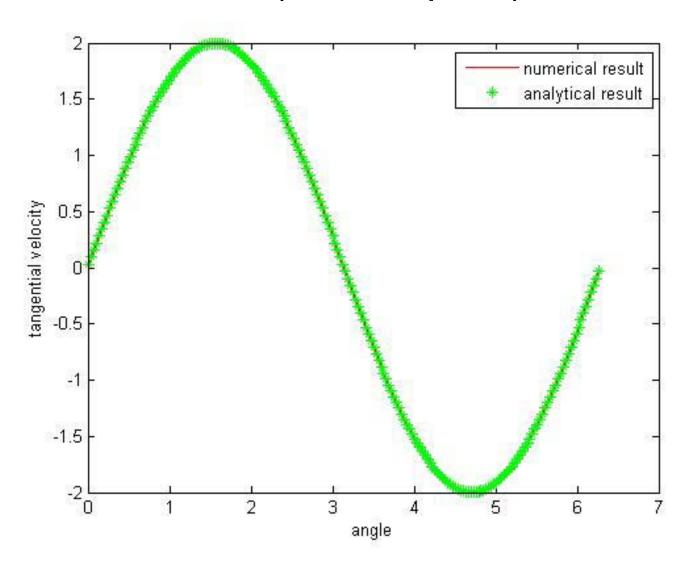
Radius of the cylinder R=2.m. The center of the cylinder at x=0 y=0 Oniferen flow speed U = 1 m/s



Comparison Between Numerical Solution and Analytic solution (NPAN=200 panels)



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