

2.25 ADVANCED FLUID MECHANICS

QUIZ 1 FALL 2004 October 14, 2004

Problem 1

A) This is a straightforward simple application of simple buoyancy ideas.

i) Force balance gives $F_R + mg = \rho g \left(\pi R^2 h + \frac{2}{3} \pi R^3 \right)$

or $F_R = \rho g \left(\pi R^2 h + \frac{2}{3} \pi R^3 \right) - mg$

for specific values given (in cgs units) $F_R = (1)(1000) \left(\pi \cdot 1^2 \cdot 5 + \frac{2}{3} \pi \cdot 1^3 \right) - 15(1000)$

$$F_R = \left(\frac{2\pi}{3} \right) (1000) = 2749 \text{ dynes}$$

ii) The 'float' is neutrally buoyant when $F_R \rightarrow 0$ then

$$mg = \rho g V_{new} = \rho g \left(\frac{2}{3} \pi R^3 + \pi R^2 h_{new} \right) \Rightarrow V_{new} = \frac{m}{\rho} = 15 \text{ cm}^3$$

If compression is slow then we can assume it is isothermal so $P_1 V_1 = P_2 V_2$ with $P_1 \cong 1 \text{ atm}$.

$$\left(\frac{P_2}{P_1} \right) = \frac{V_1}{V_2} = \frac{17\pi/3}{15} = \frac{17\pi}{45}$$

The new height of the membrane is $\frac{2}{3} \pi \cdot 1^3 + \pi \cdot 1^2 \cdot h_2 = 15 \Rightarrow h_2 = 4.107 \text{ cm}$

iii) As the pressure increases beyond this value, volume decreases further => the float valve sinks. This results in further compression of air and so it sinks further. Final resting place (labeled point '3') is on bottom of tank.

$$P_3 = P_2 + \rho g L = 1.5 P_a + \rho g L = 1.6 P_a = 1.6 \times 10^5 \text{ N/m}^2$$

Volume of air at this level is given by expression for adiabatic compression $P_3 V_3^\gamma = P_1 V_1^\gamma$

$$V_3 = V_1 (P_a / P_3)^{1/\gamma} \Rightarrow V_3 = \left(\frac{17\pi}{3} \right) \left(\frac{1}{1.6} \right)^{1/1.4} = 12.72 \text{ cm}^3$$

final height is $\frac{2}{3} \pi \cdot 1^3 + \pi \cdot 1^2 \cdot h_3 = 12.72 \text{ cm}^3 \Rightarrow h_3 = 3.38 \text{ cm}$

B) Here we must be more careful as the buoyant force concept only applies to fully submerged fraction.

For sphere to remain sitting on bottom of tank requires

$$P_T A_T + W_{sphere} + W_{water} \geq P_B \pi (R^2 - a^2) + P_a \pi a^2$$

substitute $P_T = P_a + \rho_w g(L - 2R)$, $P_B = P_a + \rho_w gL$

$$W_{water} = \rho_w g \left[\pi R^2 (2R) - \frac{4}{3} \pi R^3 \right] \quad W_{sphere} = \frac{4}{3} \pi R^3 \rho_s g = \frac{4}{3} \pi R^3 \rho_w g X$$

P_a terms cancel throughout as expected and we find:

$$\rho_w g(L - 2R)\pi R^2 + X\rho_w g \frac{4}{3} \pi R^3 + \rho_w g \left(\frac{2}{3} \pi R^3 \right) \geq \rho_w g L \pi (R^2 - a^2)$$

Canceling $\rho_w g \pi R^2$ throughout gives

$$(L - 2R) + \frac{4}{3} XR + \frac{2}{3} R \geq L(1 - a^2/R^2)$$

Or

$$X \geq 1 - \frac{3}{4} \left(\frac{L}{R} \right) \left(\frac{a^2}{R^2} \right)$$

Alternately; consider a buoyancy force arising from a displaced volume consisting of the sphere *minus* a "core" of volume $V_{core} = \pi a V_{sphere} = \pi a^2 (2R)$. We thus get a force balance of:

$$P_T \pi a^2 + \frac{4}{3} \pi R^3 X \rho_w g \geq \left[\frac{4}{3} \pi R^3 - 2R\pi a^2 \right] \rho_w g + P_a \pi a^2 \Rightarrow \text{same result!}$$

ii) For given values
$$X \geq 1 - \frac{3}{4} \left(\frac{0.8}{0.02} \right) \left(\frac{0.002}{0.02} \right)^2 = 0.70$$

As the height *decreases*, the required sphere density *increases* (otherwise the buoyant force of the displaced water upwards overwhelms the force pushing down from above).

iii) After the sphere has popped off we have a tank what is open to atmosphere and it will drain at velocity $V_{surface} = dL/dt$.

Apply steady Bernoulli equation:
$$P_a + \frac{1}{2} \rho \left(\frac{dL}{dt} \right)^2 + \rho g L = P_a + \frac{1}{2} \rho V_2^2 + 0$$

Conservation of mass gives $A_1 V_1 = A_2 V_2 \Rightarrow V_2 = V_1 \frac{A_{Tank}}{A_{Hole}} = \frac{R_T^2}{a^2} \left(\frac{dL}{dt} \right)$

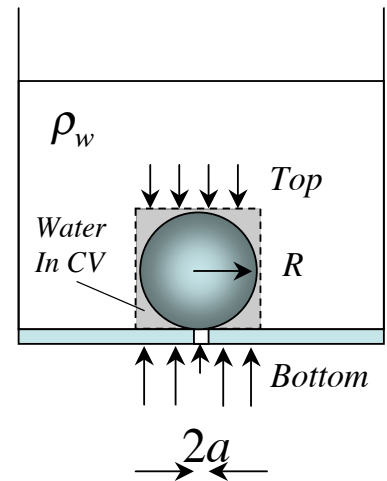
Combining gives
$$2gL = \left(\frac{dL}{dt} \right)^2 \left\{ \frac{R_T^4}{a^4} - 1 \right\}$$

Note that if the tank is an infinite reservoir then we have $V_1 \rightarrow 0$ and $V_2 \cong \sqrt{2gL}$. However this is not necessarily true in this case (and as the level drops and V_2 decreases it will become a progressively less good approximation). However for a finite size tank we need to solve:

$$\frac{dL}{dt} = - \frac{\sqrt{2gL}}{\left(R_T^4/a^4 - 1 \right)^{1/2}}$$

The solution is thus:
$$\left[\frac{1}{2} \sqrt{L} \right]_{L_0}^L = - \frac{\sqrt{2g}}{\left(R_T^4/a^4 - 1 \right)^{1/2}} t \quad \text{or} \quad L = \left\{ L_0^{1/2} - \frac{\sqrt{g/2}}{\left(R_T^4/a^4 - 1 \right)^{1/2}} t \right\}^2$$

the drainage time is
$$t_{drain} = \left(\frac{R_T^4}{a^4} - 1 \right)^{1/2} \sqrt{\frac{2L_0}{g}}$$



PROBLEM 2

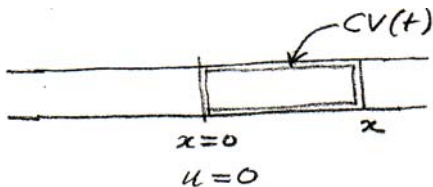
A small tube of length $2L$ is submerged in a pool of liquid (density ρ , pressure P_a). The tube is open at both ends, and filled with liquid. However, it is made of piezoelectric material, and its cross-sectional area A (which is uniform over the tube's length) can be controlled by the application of an electric voltage.

Suppose that, by the application of a suitable voltage, the tube's area is reduced in time according to a specified function $A(t)$, which is monotonically decreasing. Assuming that the flow inside the tube is incompressible and inviscid, obtain, in terms of the given quantities and the function $A(t)$ and its derivatives, expressions for

- (a) the flow speed u at a station x in the tube, and
- (b) the pressure at the tube's centerpoint, $x = 0$
- (c) Are your results in (a) and (b) valid for increasing as well as decreasing $A(t)$?

SOLUTION TO PROBLEM 2

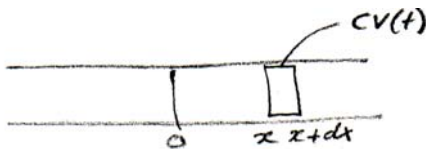
(a) simplest method for u: $\rho \frac{d}{dt}(Ax) + \rho uA = 0$



$$u = -\frac{1}{A} \frac{dA}{dt} \cdot x$$

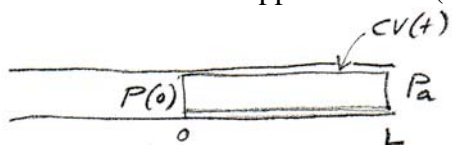
another method for u:

$$\rho \frac{\partial}{\partial t}(Adx) + \rho \frac{\partial}{\partial x}(uA)dx = 0$$



$$u = -\frac{1}{A} \frac{dA}{dt} \cdot x$$

control volume approach for $P(0)$:



$$\frac{d}{dt} \int_{cv(t)} \rho v_x dV + \int \rho v_x (\vec{v} - \vec{v}_{cs}) \cdot d\vec{A} = (P_a)_{cv}$$

$$\frac{d}{dt} \int_0^L \rho u(x,t) A dx + \rho u^2(L) A = [P(0) - P_a] A$$

Plug in for $u(x,t)$ from (a), get:

$$P(0,t) - P_a = \frac{\rho L^2}{A^2} \left(\frac{dA}{dt} \right)^2 - \frac{\rho L^2}{2A} \frac{d^2 A}{dt^2}$$

Euler equation approach for $P(0)$:

$$\begin{aligned} \frac{\partial P}{\partial x} &= -\rho \left(\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} \right) \\ &= -\rho \left[-\frac{d}{dt} \left(\frac{1}{A} \frac{dA}{dt} \right) x + \left(\frac{1}{A} \frac{dA}{dt} \right)^2 x \right] \quad \text{using (a)} \end{aligned}$$

Integrate from $x = 0$ to $x = L$, get same result.

Unsteady Bernoulli equation

$$\rho \int_0^L \frac{\partial u}{\partial t} \cdot dx + \frac{\rho u^2(L)}{2} + P_a = P(0)$$

$$u = -\frac{1}{A} \frac{dA}{dt} x \quad \text{get same thing}$$

$$P(L) \cong P_a - \frac{1}{2} \rho u^2(L) \quad \text{as first approximation.}$$

Answer in (a) OK, answer in (b) must be modified to account for different $P(L)$, as indicated above.