are in the ratio of 2:1.

JAWAHARLAL NEHRU TECHNOLOGICAL UNIVERSITY HYDERABAD Code No: 126EF B.Tech III Year II Semester Examinations, May - 2016

HEAT TRANSFER

| D. Z | HEAT TRANSPOR | | |
|--|--|---------------------------------------|---|
| | Common to ME, AME, MSNT) | Max. Ma | arks: 75 |
| | 302 | | * *** |
| Time: 3 hours | | | |
| *** **** x | nins two parts A and B. nich carries 25 marks. Answer al wer any one full question from ea | | A. Part B |
| This question paper conta | ins two parts amarks. Answer al | il questions in raction | on carries |
| Note: This question will be a secompulsory wh | nich carries 25 marks | ch unit. Each questic | JII Cur |
| Part A is conf | ver any one full question | | |
| consists of 5 officer | nich carries 25 marks. Answer al wer any one full question from ea a, b, c as sub questions. | | *** ***** |
| consists of 5 Units. Answ 10 marks and may have a | | * * * * * * * * * * * * * * * * * * * | *** *** |
| | PART - A | (2 | 5 Marks) |
| | 1.xx 2 2 x | | |
| | | | [2] |
| | | | [3] |
| 1.a) Define thermal diffusivi | ty. etween homogeneous and isotrophite body. | pic material. | [2] |
| 1.a) Define the difference b | etween homogeneous and | *** **** | ::::::::::::::::::::::::::::::::::::::: |
| b) What is the different infil | nite body. | cal significance. | |
| c)Discuss about sent from | ier numbers? Explain their physic | n heat transfer proce | ss. [2] |
| d) What are Biot and roun | nite body. ier numbers? Explain their physical ication of dimensional analysis is lication of dimensional analysis in the second | 1 turbulent flows in | a pipe and |
| e) State the scope and app | nite body. ier numbers? Explain their physic lication of dimensional analysis i growth in a pipe for laminar and | 1 turbulone 22 | [3] |
| Describer to the second | 0 | | [2] |
| f) Draw boundary indicate salient features | 3. | • • • • • | [3] |
| | | ise condensation? | ::: [2] |
| g) Define madiate | radiosity. es between drop wise and film wi between regenerator and recuper | ator? : | [3] |
| h) what are the difference | between regenerator and recap- | | [و] |
| i): What is the difference i) What is LMTD correc | es between drop wise and filling who between regenerator and recuper tion factor? | | |
| j) What is LMTD correc | | | |
| | PART - B | | (50 Marks) |
| | | *** | ******* |
| | | | *4× × |
| AND SERVICE CONTRACTOR OF THE PROPERTY OF THE | onduction equation in Cartesian (anduction shape factor? Explain it | Co-ordinates. | with periodic |
| Derive general heat c | onduction equation in factor? Explain it | s significance along | [5+5] |
| TATI -4 to meall IV COL | | | LO. |
| b) What is meant of and aperiodic heat tra | insfer. | | |
| and aperiodic ness | OR | iscuss the conditions: | *** **** |
| of in | oR itial and boundary conditions? Di | ×ו *•ו | *** |
| 3. What is the use of m | a temperature | **** | |
| Desceribed Surface | | | [3+3+4] |
| b) Prescribed Heat 11 | | | |
| b) Prescribed fleat in c) Convective condi- | tion in detail. neat transfer coefficient? Obtain the convective conditions over the | for C | omposite wall |
| | cciaint? ()htain | the expression for c | Omp |
| Define the overall h | neat transfer coefficients over the | wall | 6+41 |
| 4.a) Define the overall | neat transfer coefficient? Obtain th convective conditions over the n steady state conduction and uns | steady state conduction | on. Estatoria |
| with three rayons | n steady state conduction and and | | •=1 |
| Distinguish Detwee | OD | | gle material. |
| the state of the s | dictribution a | | - I he mile |
| 5.a) Develop an express | sion for temperature distributed and steel, each of thickness 1cm kept at 100°C and the outer surthe common interface? The ther | , are placed in kent | at 0°C. What is |
| b) Sheets of brass ar | kept at 100°C and the outer surthe common interface? The ther | face of sieer is repe | f brass and steel |
| b) Sheets of brass is | kept at 100 C and and The ther | mal conductivities of | |
| Surface of stora of | the common interface. | *** | ** 1 LT . T-4 |

the temperature of the common interface? The thermal conductivities of brass and steel

- 6.a): Differentiate between mechanisms of heat transfer by free and forced convection.

 Mention some of the areas where these mechanisms are predominant.
 - b) A nuclear reactor with its core constructed of parallel vertical plates 2.25 m high and 1.5 wide has been designed on free convection heating of liquid bismuth. Metallurgical considerations limit the maximum surface temperature of the plate to 975° C and the lowest allowable temperature of bismuth is 325° C. Estimate the maximum possible heat dissipation from both sides of each plate. The appropriate correlation for the convection coefficient is $Nu = 0.13(Gr \text{ Pr})^{\frac{1}{3}}$ where the different parameters are evaluated at the mean film temperature. [5+5]

OR

7.a) How are the local and average convection coefficients for flow past a flat plate are

Water at 75° C flows through a 0.005 m diameter tube with a velocity of 1m/s. If the tube wall temperature is 25° C, make calculations for the heat transfer coefficient. Use the correlation, St = 0.023 Re $^{0.2}$ Pr $^{-0.667}$.

The thermo-physical properties of water are:

Thermal conductivity is 0.647 W/(m.K); Viscosity is 1.977 kg/h.m;

Density is 1000 kg/m³; Specific heat 4.187 kJ/(kg.K).

[5+5]

- 8.a) What is Stefan-Boltzmann Law? Explain the concept of total emissive power of a surface.
- b) Saturated steam at 2 bar condenses on a cylindrical vertical drum having an outside diameter of 25 cm and a temperature of 90° C. Calculate how long must the drum be to condense 50 kg of steam per hour. Also estimate the thickness of condensate layer.

[5+5]

OR

- 9.a) Derive general relation for the radiation shape factor in case of radiation between two surfaces.
 - b). ... A copper pan of 35 cm diameter contains water and its bottom surface is maintained at 115° C by an electric heater. Calculate the power required to boil water in this pan and the rate at which water evaporates from the pan due to the boiling process. Also make calculations for the heat flux for these conditions. [5+5]
- 10. It is required to design a shell and tube heat exchanger for heating 9000 kg/hr of water from 15°C to 88°C by hot engine oil (Cp = 2:35 kJ/kg-K) flowing through the shell of the heat exchanger. The oil makes a single pass, entering at 150°C and leaving at 95°C with an average heat transfer coefficient of 400 W/m²-K, the water flow through 10 thin walled tubes of 25mm diameter with each tube making 8 passes through the shell. The heat transfer efficient on the water side is 3000 W/m²-K. Find the length of the tube required for the heat exchanger.

OR

- 11:a) Derive an expression for LMTD in case of a counter current flow double pipe heat exchanger.
 - b) A hot fluid enters a heat exchanger at a temperature of 200°C at a flow rate of 2.8 kg/sec (sp. heat 2.0 kJ/kg-K) it is cooled by another fluid with a mass flow rate of 0.7 kg/sec (Sp. heat 0.4 kJ/kg-K). The overall heat transfer coefficient based on outside area of 20 m² is 250 W/m²-K. Calculate the exit temperature of hot fluid when fluids are in parallel flow. [5+5]